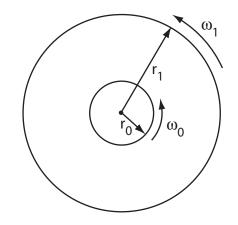
Problem #1

Assume:

- Incompressible •
- 2-D flow $\Rightarrow V_z = 0, \frac{\partial}{\partial z} = 0$
- Steady $\Rightarrow \frac{\partial}{\partial t} = 0$ Parallel $\Rightarrow V_r = 0$ •
- •
- a) Conservation of mass for a 2-D flow is:

$$\frac{1}{r}\frac{\partial}{\partial r}(r\underbrace{X}_{\theta}) + \frac{1}{r}\frac{\partial}{\partial \theta}(V_{\theta}) = 0$$
$$\Rightarrow \frac{\partial}{\partial \theta}(V_{\theta}) = 0 \Rightarrow V_{\theta} \text{ does not depend on } \theta$$
$$\Rightarrow \boxed{V_{\theta} = V_{\theta}(r)}$$



b) θ -mometum equation is:

$$\frac{\partial V_{\theta}}{\partial t} + (\vec{V} \cdot \nabla)V_{\theta} + \underbrace{\frac{\nabla V_{\theta}}{r}}_{V_{r}=0} = -\frac{1}{\rho r}\frac{\partial p}{\partial \theta} + \nu(\nabla^{2}V_{\theta} + \frac{2}{r^{2}}\underbrace{\frac{\partial V_{r}}{\partial \theta}}_{V_{r}=0} - \frac{V_{\theta}}{r^{2}})$$

In cylindrical coordinates:

$$(\vec{V} \cdot \nabla) = \underbrace{\bigvee_{i=0}}_{\sigma} \frac{\partial}{\partial r} + \frac{1}{r} V_{\theta} \frac{\partial}{\partial \theta}$$

Thus,

$$(\vec{V} \cdot \nabla)V_{\theta} + \frac{1}{r}V_{\theta} \underbrace{\underbrace{\partial V_{\theta}}_{\substack{=0 \text{ from}\\ \text{continuity}}}} = 0$$

Also,

$$\nabla^2 V_{\theta} = \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial V_{\theta}}{\partial r} \right) + \underbrace{\frac{1}{r^2} \frac{\partial^2 V_{\theta}}{\partial r^2}}_{=0}$$

Combining all of these results gives:

$$\frac{1}{\rho r} \frac{\partial p}{\partial \theta} = \underbrace{\nu \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial V_{\theta}}{\partial r} \right) - \frac{V_{\theta}}{r^2} \right]}_{\text{this side is independent of } \theta}$$

Since the right-hand-side (RHS) is independent of θ , this requires that $\frac{\partial p}{\partial \theta} = \text{constant}$ for fixed r. But as θ varies from $0 \rightarrow 2\pi$, it must be equal at $0 \& 2\pi$, that is $p(\theta = 0) = p(\theta = 2\pi)$. If not, the solution would be discontinuous. Thus, $\frac{\partial p}{\partial \theta} = 0 \Leftarrow \text{ constant}$ must be zero!

The differential equation for V_{θ} is:

$$\frac{1}{r}\frac{\partial}{\partial r}\left(r\frac{\partial V_{\theta}}{\partial r}\right) - \frac{V_{\theta}}{r^{2}} = 0$$

A little rearranging gives:

$$\frac{d}{dr} \left[\frac{1}{r} \frac{d}{dr} (rV_{\theta}) \right] = 0$$

Integrating once gives:

$$\frac{1}{r}\frac{d}{dr}(rV_{\theta}) = C_1$$

Integrating again gives:

$$rV_{\theta} = \frac{1}{2}C_{1}r^{2} + C_{2}$$
$$\Rightarrow V_{\theta} = \frac{1}{2}C_{1}r + \frac{C_{2}}{r}$$

Next, we must apply the no-slip boundary conditions to find V_{θ} . Specifically,

at
$$r = r_o$$
, $V_{\theta} = \omega_o r_o$
at $r = r_1$, $V_{\theta} = \omega_1 r_1$

because flow velocity equals wall velocity in a viscous flow.

So, apply $r = r_o \& r = r_1$ bc's:

$$\omega_{o}r_{o} = \frac{1}{2}C_{1}r_{o} + \frac{C_{2}}{r_{o}} \\ \omega_{l}r_{l} = \frac{1}{2}C_{1}r_{l} + \frac{C_{2}}{r_{l}} \\ \Rightarrow \begin{cases} \frac{1}{2}C_{1} = \frac{\omega_{l}\frac{r_{1}}{r_{o}} - \omega_{o}\frac{r_{o}}{r_{1}}}{\frac{r_{1}}{r_{o}} - \frac{r_{0}}{r_{1}}} \\ \Rightarrow r_{0} - r_{1} \\ C_{2} = \frac{r_{o}r_{1}(\omega_{o} - \omega_{1})}{\frac{r_{1}}{r_{0}} - \frac{r_{0}}{r_{1}}} \end{cases}$$

Or, rearranged a little gives:

$$V_{\theta} = r_{o}\omega_{o}\frac{\frac{r_{1}}{r_{o}} - \frac{r_{r_{1}}}{r_{1}}}{\frac{r_{o}}{r_{o}} - \frac{r_{o}}{r_{1}}} + r_{1}\omega_{1}\frac{\frac{r_{o}}{r_{o}} - \frac{r_{o}}{r_{0}}}{\frac{r_{o}}{r_{1}} - \frac{r_{o}}{r_{0}}}$$

c) The radial momentum equation is:

$$\frac{\partial V_r}{\partial t} + (\vec{V} \cdot \nabla) V_r - \frac{1}{r} V_{\theta}^2 = -\frac{1}{\rho} \frac{\partial p}{\partial r} + \nu \left(\nabla^2 V_r - \frac{V_r}{r^2} - \frac{2}{r^2} \frac{\partial V_{\theta}}{\partial \theta} \right)$$

But $V_r = 0$ & $\frac{\partial V_{\theta}}{\partial \theta} = 0$ so this reduces to:

$$\frac{\partial p}{\partial r} = \frac{\rho V_{\theta}^2}{r}$$

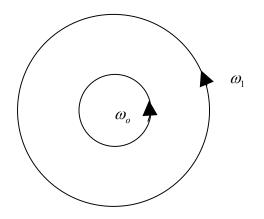
Since $\frac{\rho V_{\theta}^2}{r} \ge 0$ always, then clearly $\frac{\partial p}{\partial r} \ge 0$.

Thus, pressure increases with r.

d) On the inner cylinder, the moment is a result of the skin friction due to the fluid shear stress. For this flow in which only $V_{\theta} \neq 0$ and is only a function of r, the only non-zero shear stress is $\tau_{r\theta}$ and has the following form:

$$\tau_{r\theta} = \mu \underbrace{\left(\frac{\partial V_{\theta}}{\partial r} - \frac{V_{\theta}}{r}\right)}_{=\varepsilon_{r\theta}, \text{ the only}} = \mu \left[r\frac{\partial}{\partial r}\left(\frac{V_{\theta}}{r}\right)\right]$$

Rotating Cylinders



For the problem you studied in the homework:

1. What direction is the fluid element acceleration?

2. What direction are the net pressure forces on a fluid element?

3. What direction are the net viscous forces on a fluid element?